

Fuel Cell Workshop: Part I

Education Department, HKSAR &

Department of Chemistry
The University of Hong Kong

September/October 2003

Sir William Grove 1839

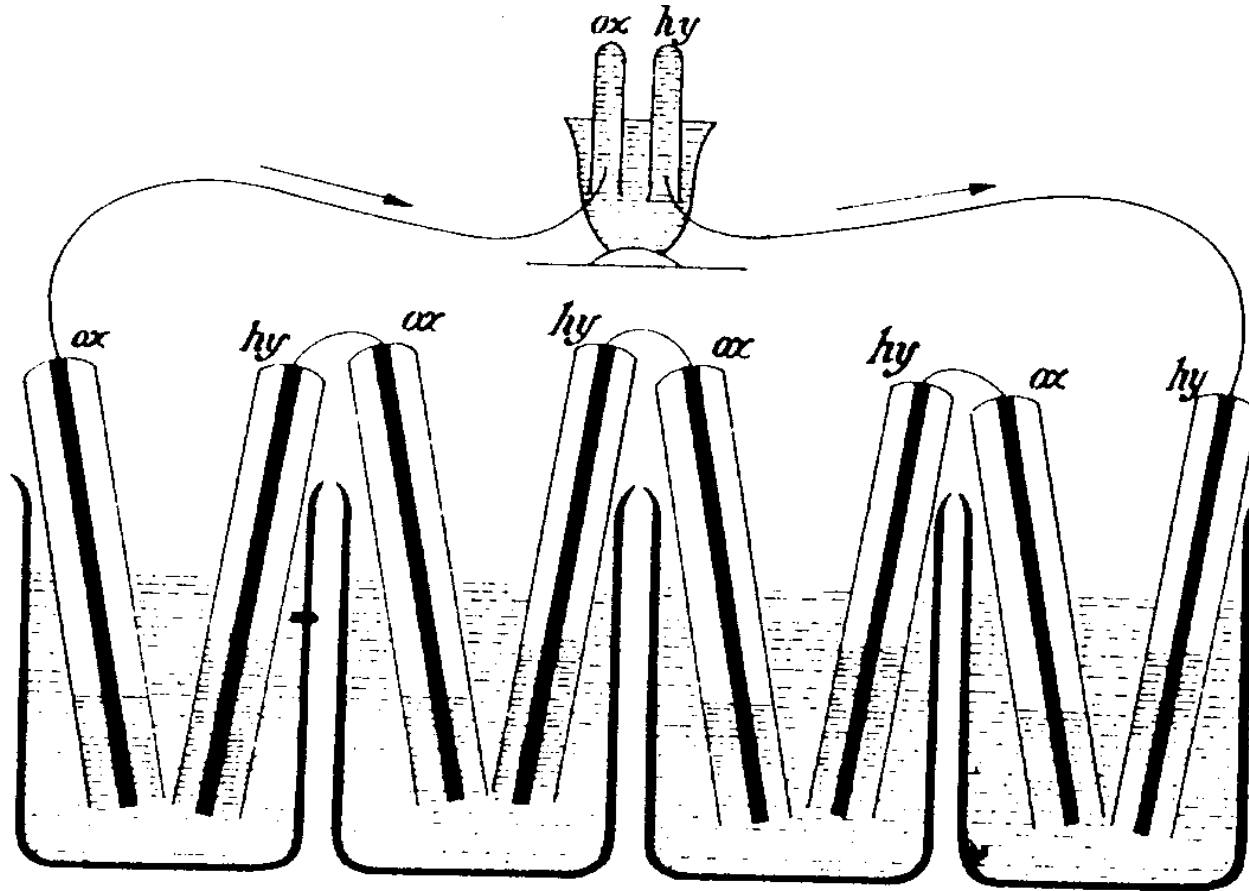


Fig. 1.5 *Four cells of Groves H₂/O₂ battery, used, in Grove's words, 'to effect the decomposition of water by means of its composition'*

Batteries Vs Fuel Cells

Batteries

- Recharge
- Intermittent
- Closed system
- Mostly solid
- High power density

Fuel Cells

- ReFuel
- Continuous
- Open system
- Mostly Gas/Liquid Fuel
- High energy density
- Micro to Mega Watts

Types of Fuel Cells

Classification according to electrolyte

- Alkaline Fuel Cells (AFC)
- Proton Exchange Membrane (PEM)
- Phosphoric Acid (PAFC)
- Molten Carbonate (MCFC)
- Solid Oxide Electrolyte (SOFC)

Classification according to fuel-oxidant

- Hydrogen-oxygen
- Direct methanol (DMFC)
- Hydrogen-bromine

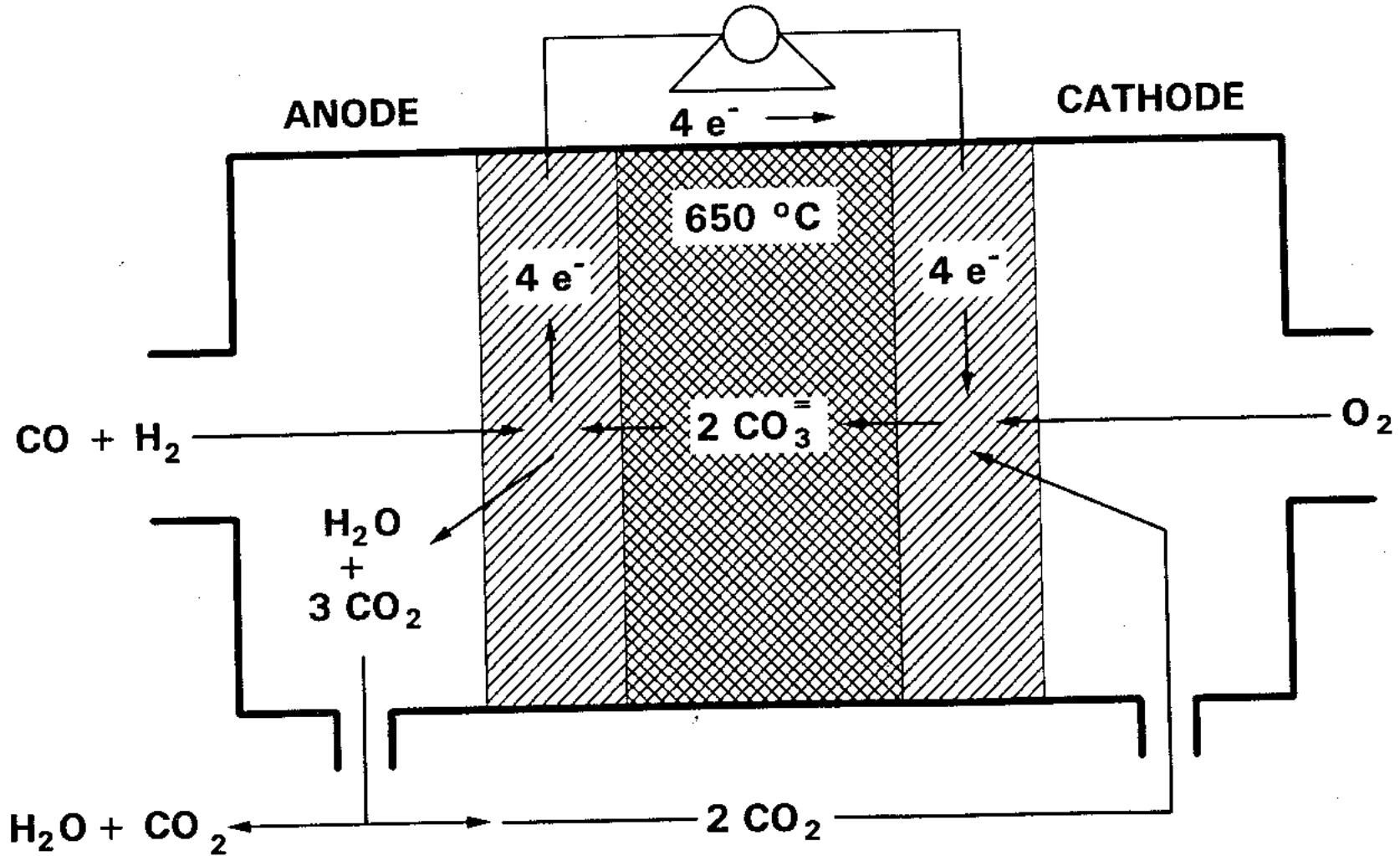
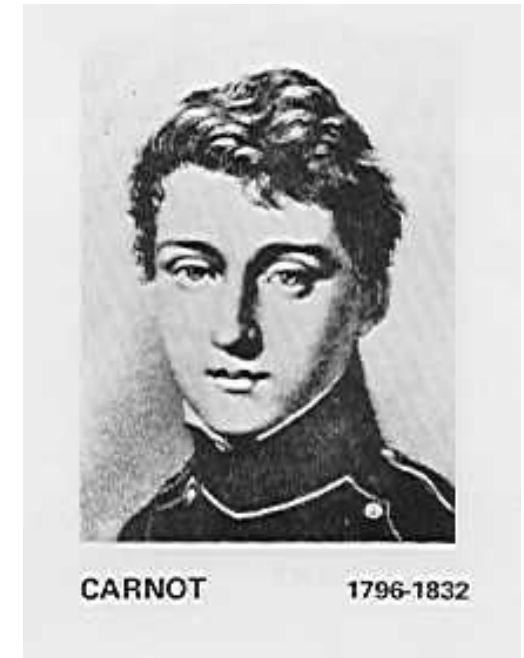
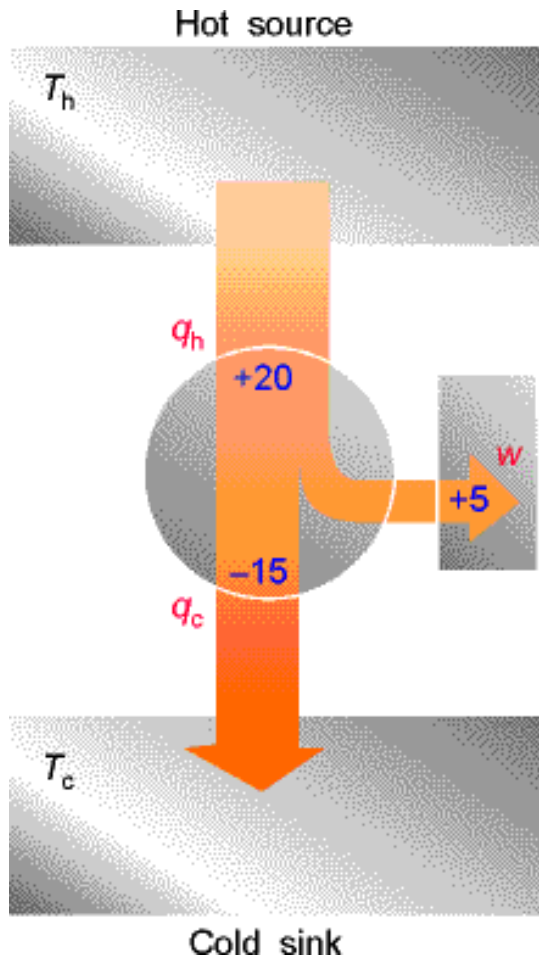


Figure 2.8. Schematic of a molten carbonate fuel cell.

Advantages of Fuel Cells

- Efficient conversion of Chemical Energy to useful energy (without losing to heat, mechanical linkages)
- Environmentally friendly
- Flexible: from micro to mega
- Continuous or Rapid refueling for portable use
- Quiet: for military applications



Carnot's Theorem

Efficiency of Heat Engine

$$\eta_{\text{thermal}} = \frac{\text{Work}}{\text{Heat}} = 1 - \frac{T_c}{T_h}$$

Fuel Cells

Chemical Energy \longrightarrow Electrical Energy

$$\eta_{\text{thermal}} = \frac{\text{Work}}{\text{Heat}} = \frac{\Delta G}{\Delta H} = \frac{\Delta H - T\Delta S}{\Delta H}$$

Thermodynamics

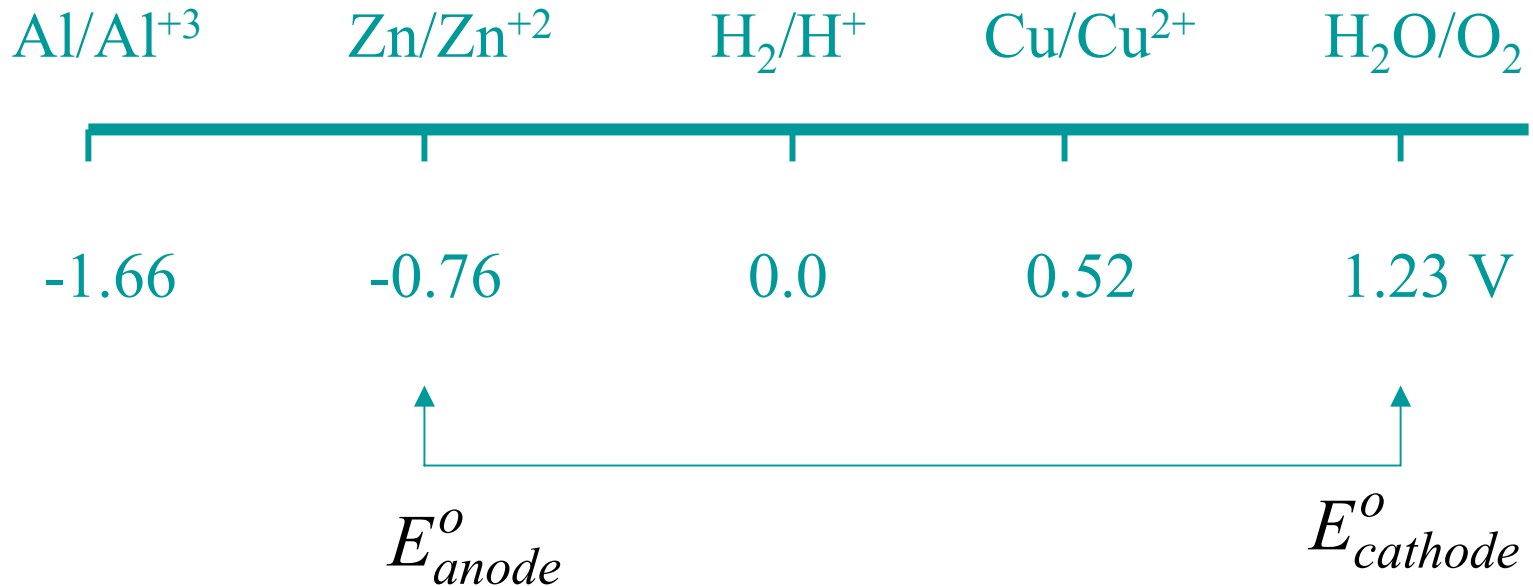
- Relate Reactivity to **Electrode Potential**
- **Nernst Equation** accounts for concentration(activity) effects

$$E - E^{\circ} = -\frac{RT}{nF} \ln \left[\frac{a_C^c a_D^d}{a_A^a a_B^b} \right] \approx \frac{-0.0591}{n} \log \frac{[Re]}{[Ox]}$$

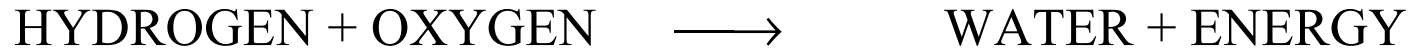
- Calculate Electrode Potential from **Free Energy**

$$E_{cathode}^{\circ} - E_{anode}^{\circ} = E_{cell}^{\circ} = -\frac{\Delta G^{\circ}}{nF}$$

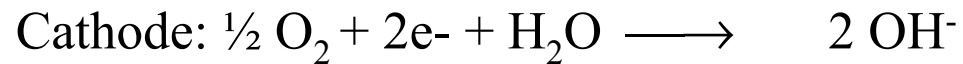
Electrochemical Activity Series



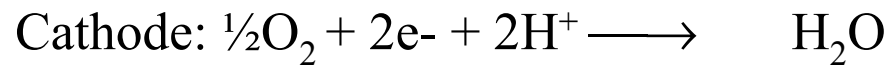
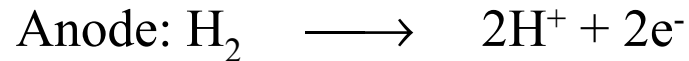
$$E^\circ_{cathode} - E^\circ_{anode} = E^\circ_{cell} = -\frac{\Delta G}{nF}$$



Alkaline

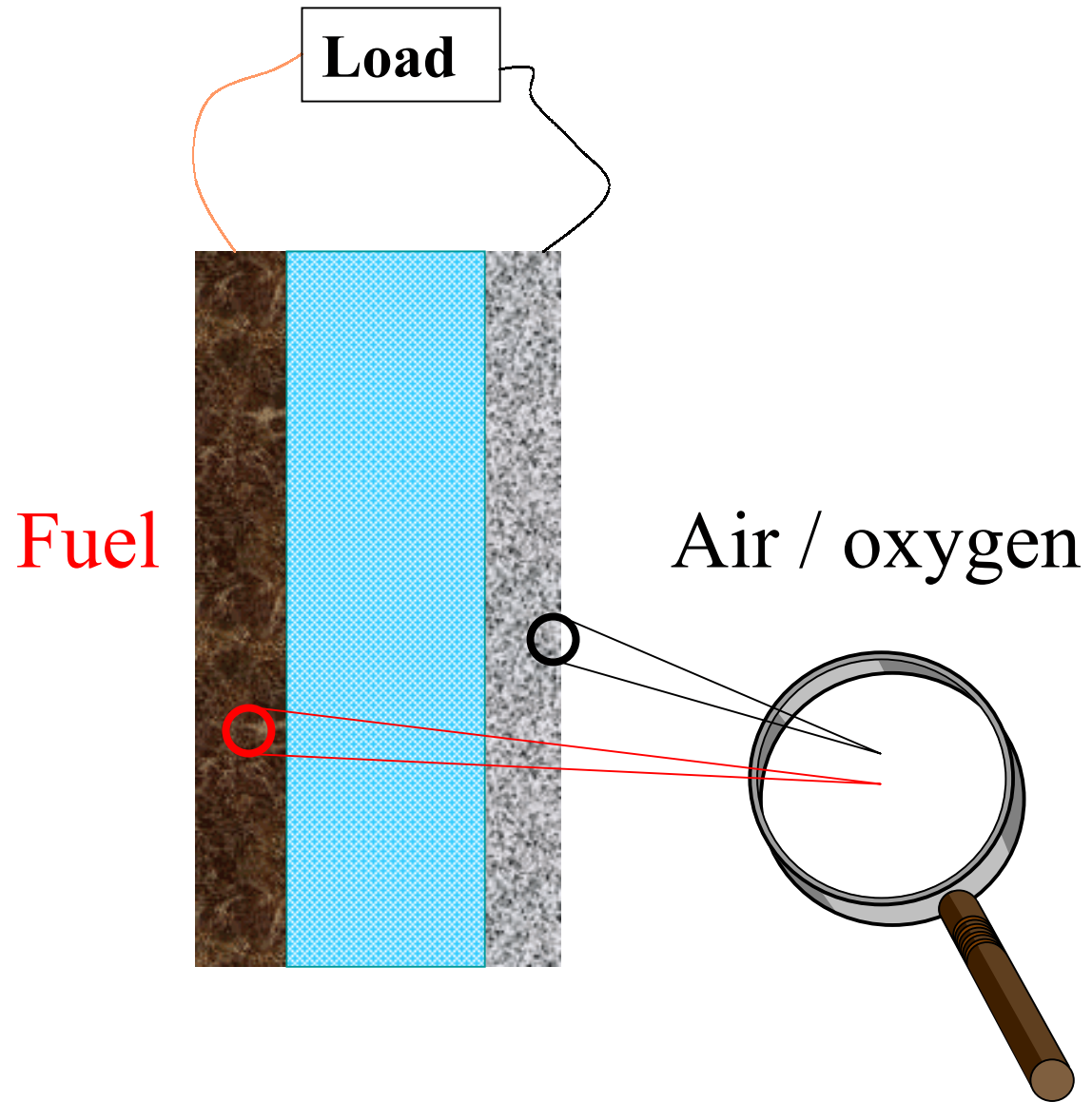


Acidic



Thermochemistry

	$\Delta_c H^\circ$ (kJmol ⁻¹)	$\Delta_c G^\circ$ (kJmol ⁻¹)	n	E°	kJ/kg	kJ/cm ³
Hydrogen	- 285	- 237	2	1.23	118500	10.65
Carbon	- 395	- 394				
Methane	- 890	- 818	8	1.06	51125	
Ethane	-1560	-1467				
Methanol	- 726	- 702	6	1.21	21938	17.37
Glucose	-2808	-2865	24	1.23	15916	24.57
Octane	-5471				47907	



Fuels: Hydrogen
Metals
Natural Gas
Small Hydrocarbons
(methanol, glucose)

Oxidant: air
oxygen
halides
oxides

Catalysts: platinum
metals
metal oxides
macrocycles

Catalyst Support:
Porous Carbon
Ceramic Matrix
Metal Foam
PTFE

Bipolar Plate, Frame, container.

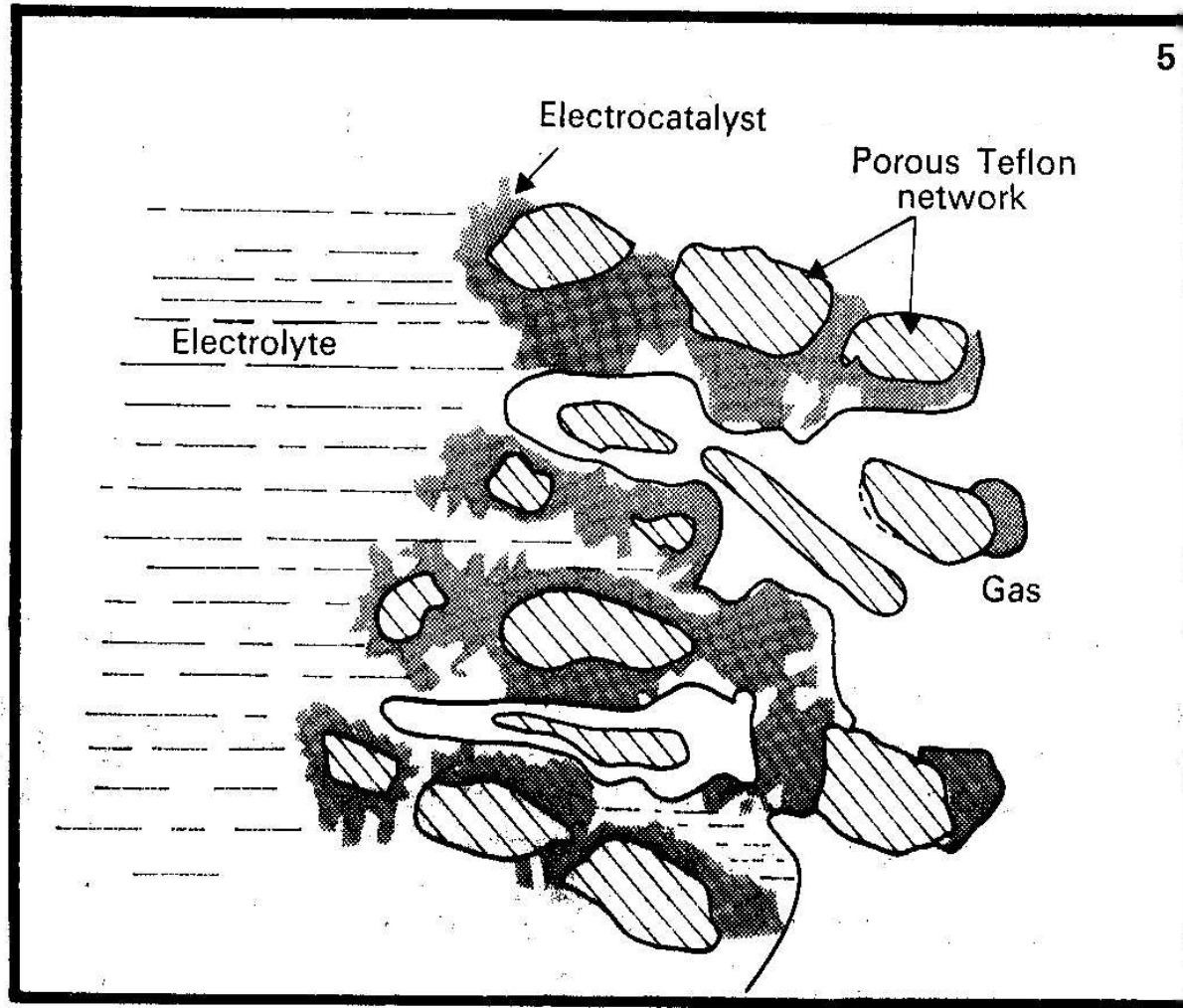
Electrolyte:
Porous Matrix
Proton Exchange Membranes
Yttrium stabilized Zirconia

Storage: Metal Hydride

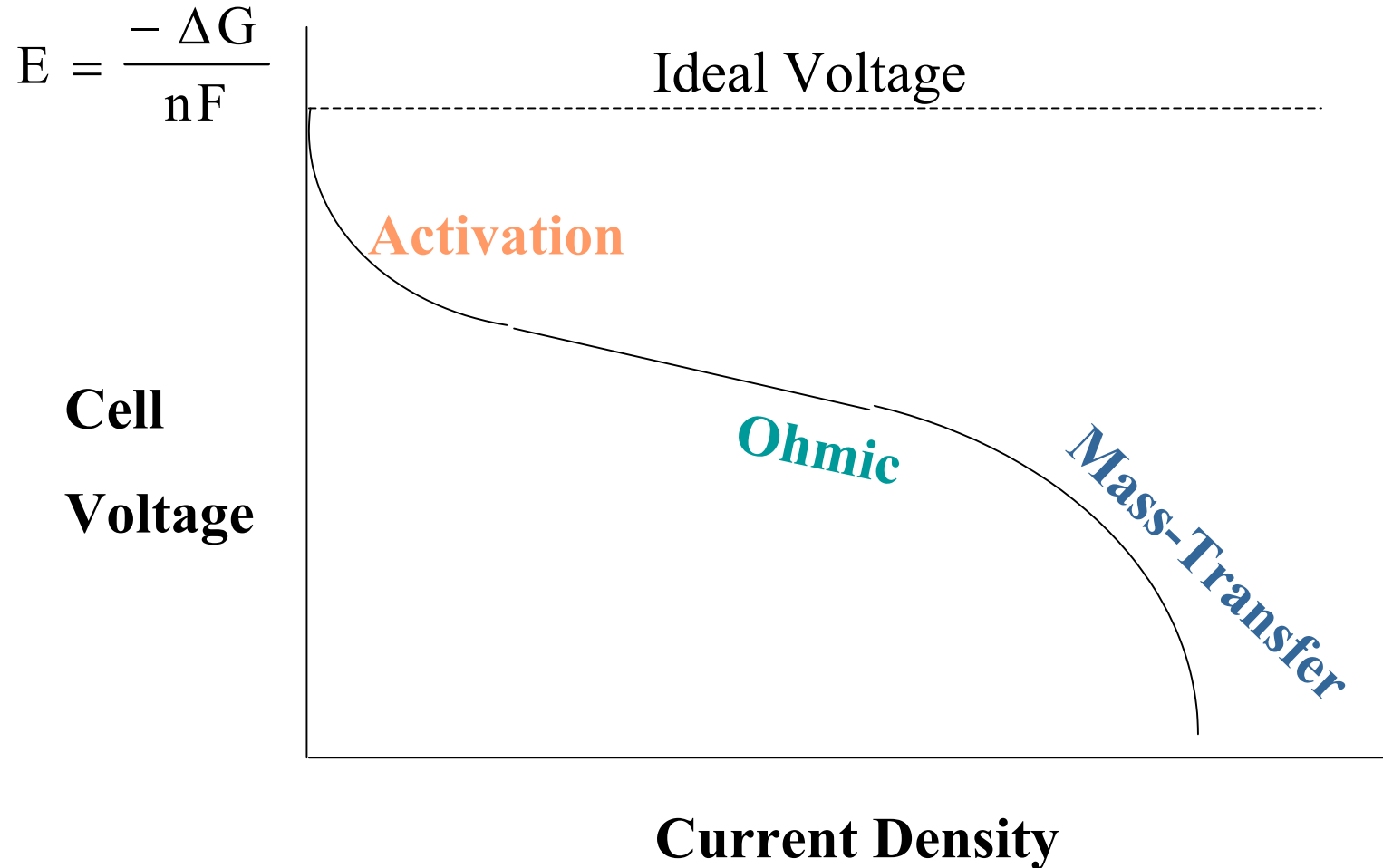
Electrodes:

- Catalyst Support: High Surface Carbon
- Size Effects of Catalysts
- Controlled Porosity
- Controlled Wetting
- Maximum Gas-Liquid-Solid Interface
- Minimize ohmic resistance
- Minimize ionic resistance

Gas Diffusion Electrode: PTFE bonded electrode



Performance of a Fuel Cell



$$E^{\circ}_{\text{cell}} = -\Delta G / (nF)$$

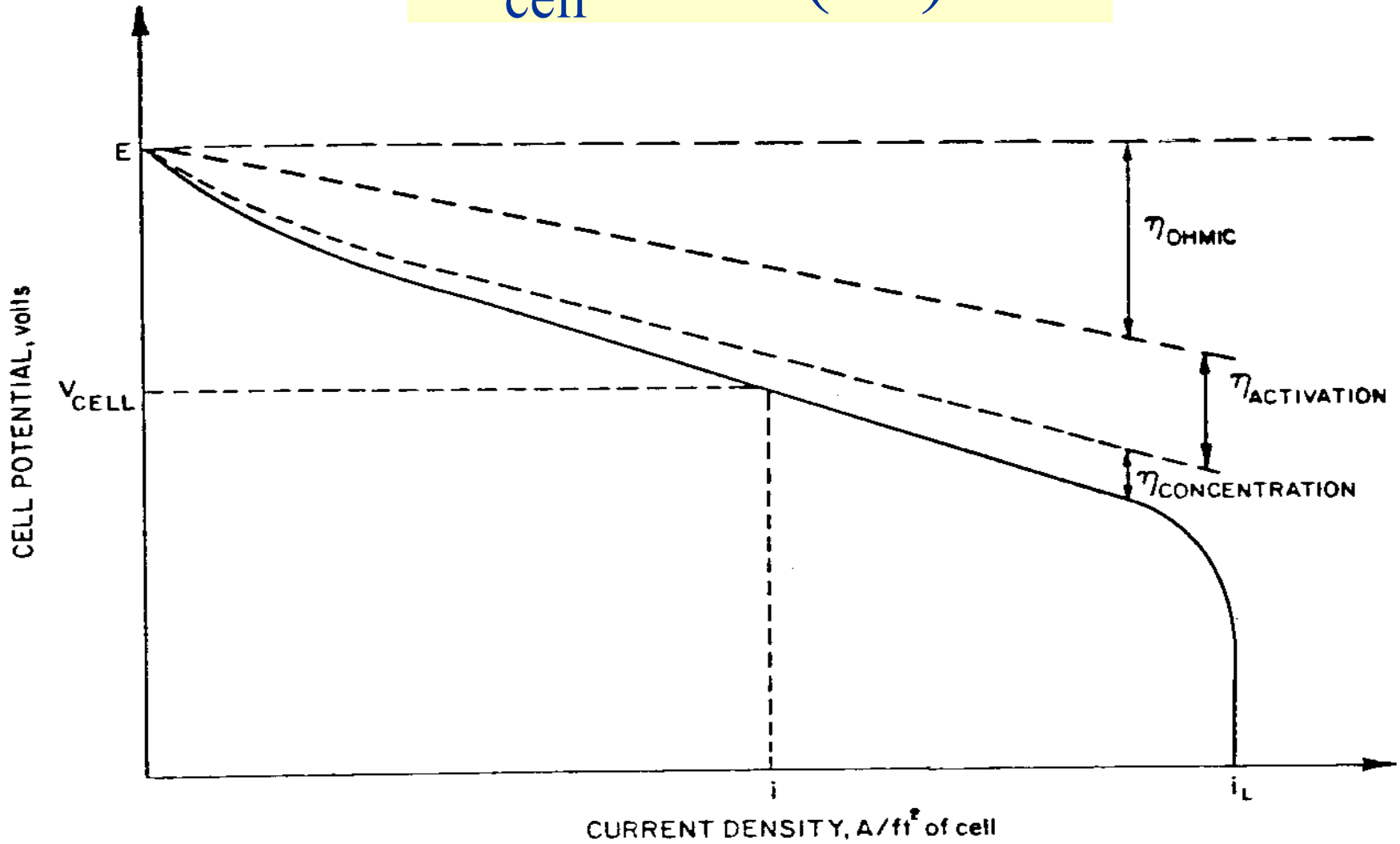


Figure 2.1. SCHEMATIC FUEL CELL POLARIZATION CURVE

A79061304

Electrode Kinetics

- Current \propto Rate of reaction (Faraday's law)
- Rate (current) described by **Tafel Equation**

$$E - E^{eq} = \frac{RT}{\alpha nF} \ln i + const._o$$

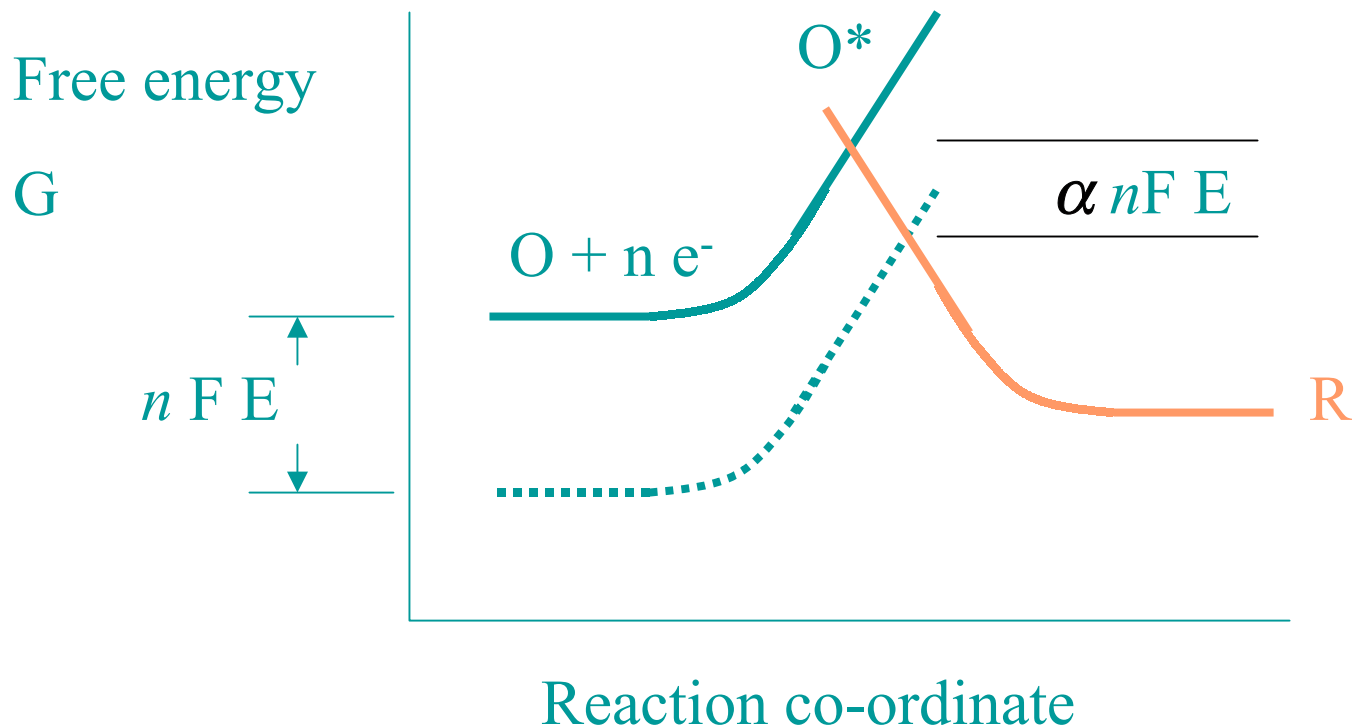
or Butler-Volmer Equation (Bard and Faulkner, Wiley 2001)

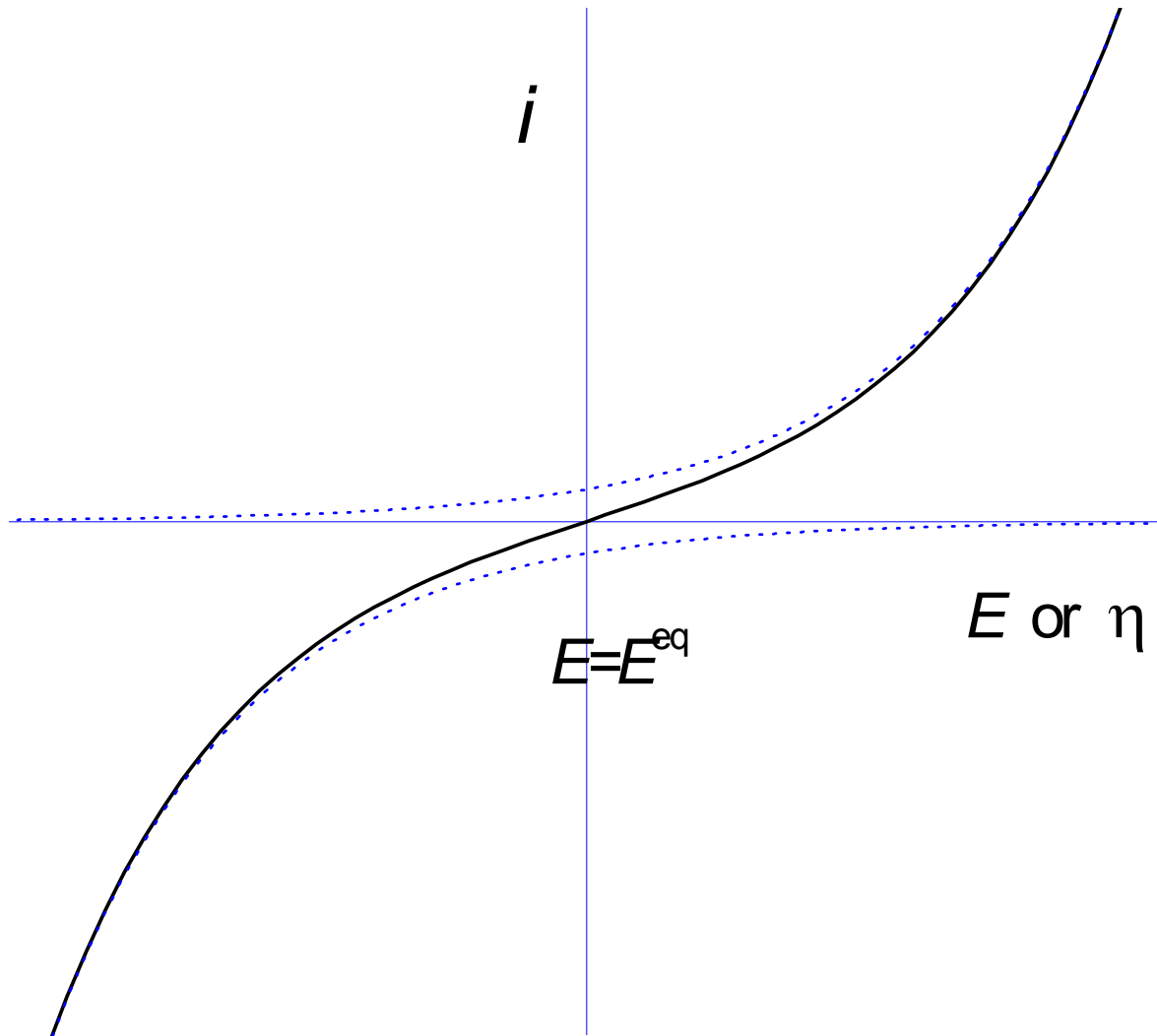
$$i = i_o \left\{ \frac{C_O}{C_O^*} \exp\left[\frac{-\alpha nF(E - E^{eq})}{RT} \right] - \frac{C_R}{C_R^*} \exp\left[\frac{(1 - \alpha)nF(E - E^{eq})}{RT} \right] \right\}$$

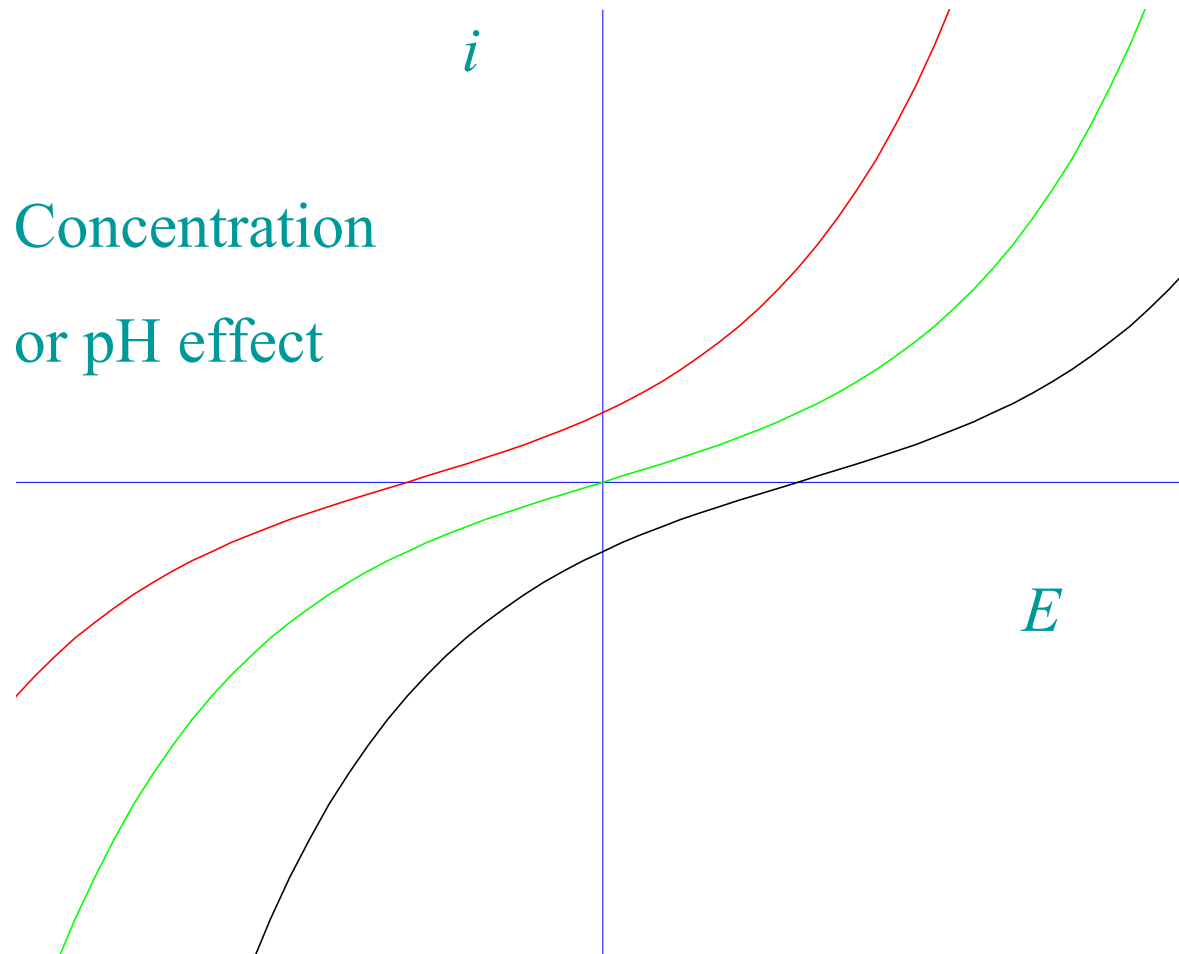
Electrode Kinetics

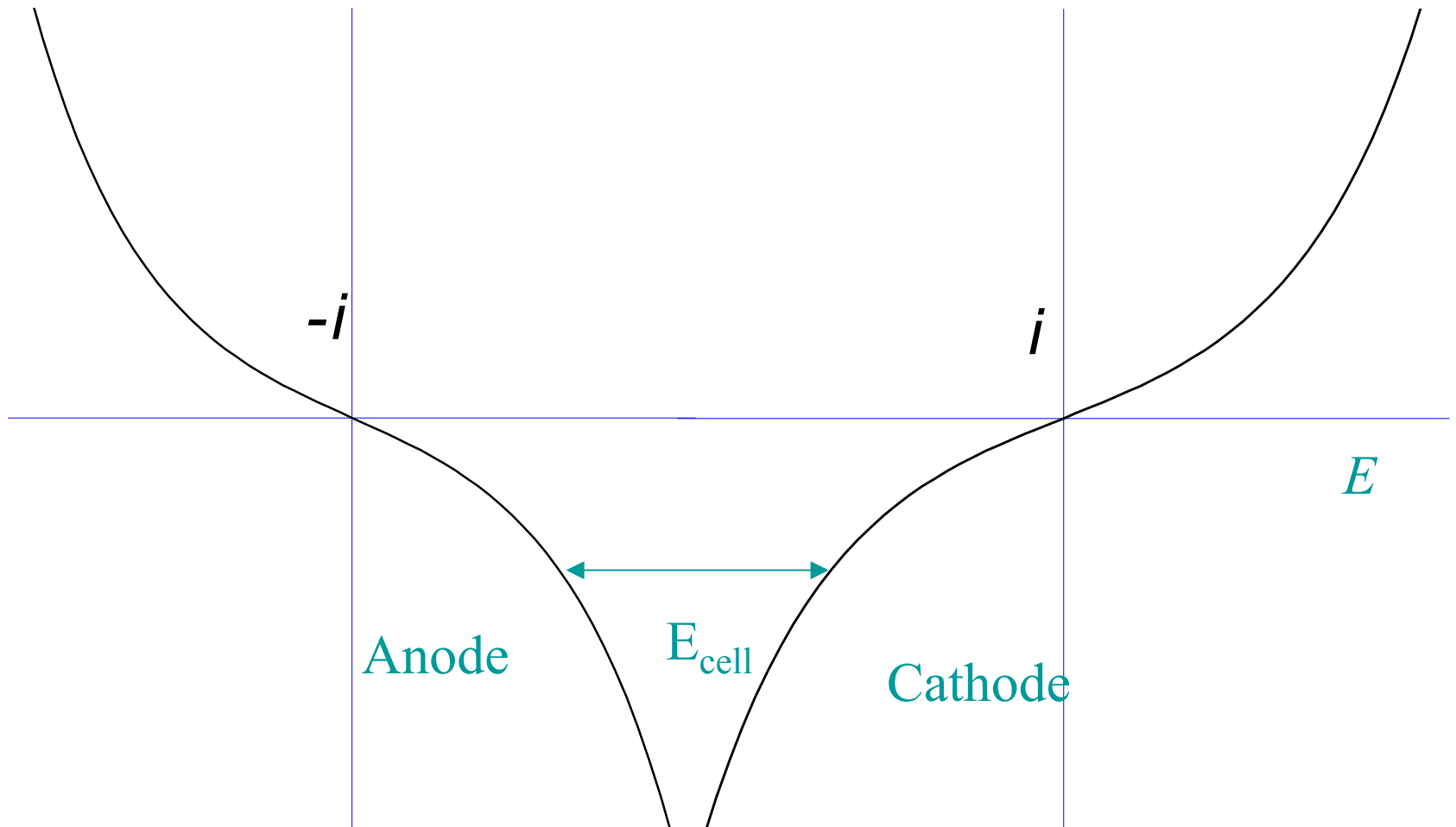
$$i = i_o \left\{ \frac{C_O}{C_O^*} \exp\left[\frac{-\alpha n F (E - E^{eq})}{RT} \right] - \frac{C_R}{C_R^*} \exp\left[\frac{(1-\alpha) n F (E - E^{eq})}{RT} \right] \right\}$$

from Absolute Rate Theory







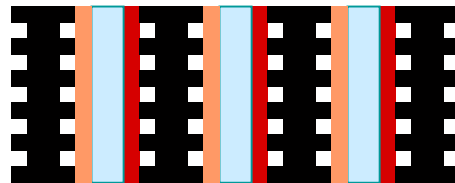
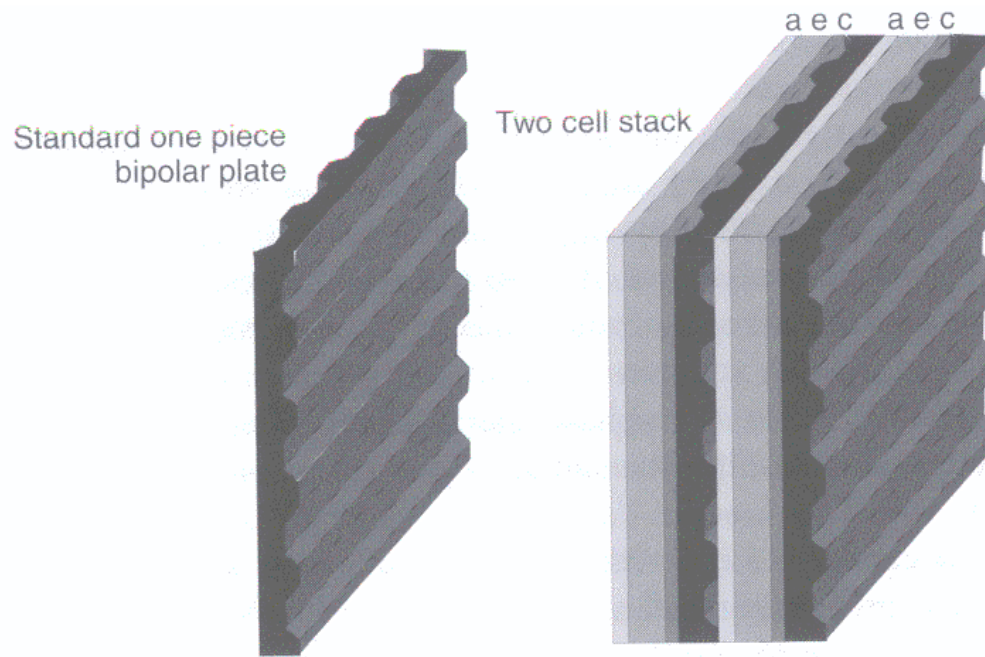


Tests Other than Polarization Curve:

- Half Cell Study (3 Electrode set up)
- Chronopotentiometry
- Chronoamperometry

Stack Design

- Manifold for fuel feed
- Manifold for oxidant feed
- Electronic circuit
- Ionic circuit
- Water transport
- Temperature, humidity control



H^+

Stationery Power Utilities

10~100 kW

100~500 kWhr

ONSY (IFC), Fiji

SOFC (Westing House, Honey Well)

Load Levelling

Power Distribution

Life



Portable Power Sources

10~100 kW

100~500 kWhr

Battery vs Fuel Cells

Safety (H_2 , MeOH, caustic electrolyte),
Open vs Closed System

Volume vs Weight

Refueling Vs Recharging

Electric Vehicles

10~100 kW

100~500 kWhr

Battery vs Fuel Cells

Hybrid with ICE and capacitor

Costs: 7 times normal costs

Startup time

Direct/Reformer

Fueling Station Infrastructure









Special Applications

Defence

Communication

Energy Storage for Solar, Wind

Energy Vector

Biomedical

Energy Recovery from Waste

Marine and Remote Power Sources

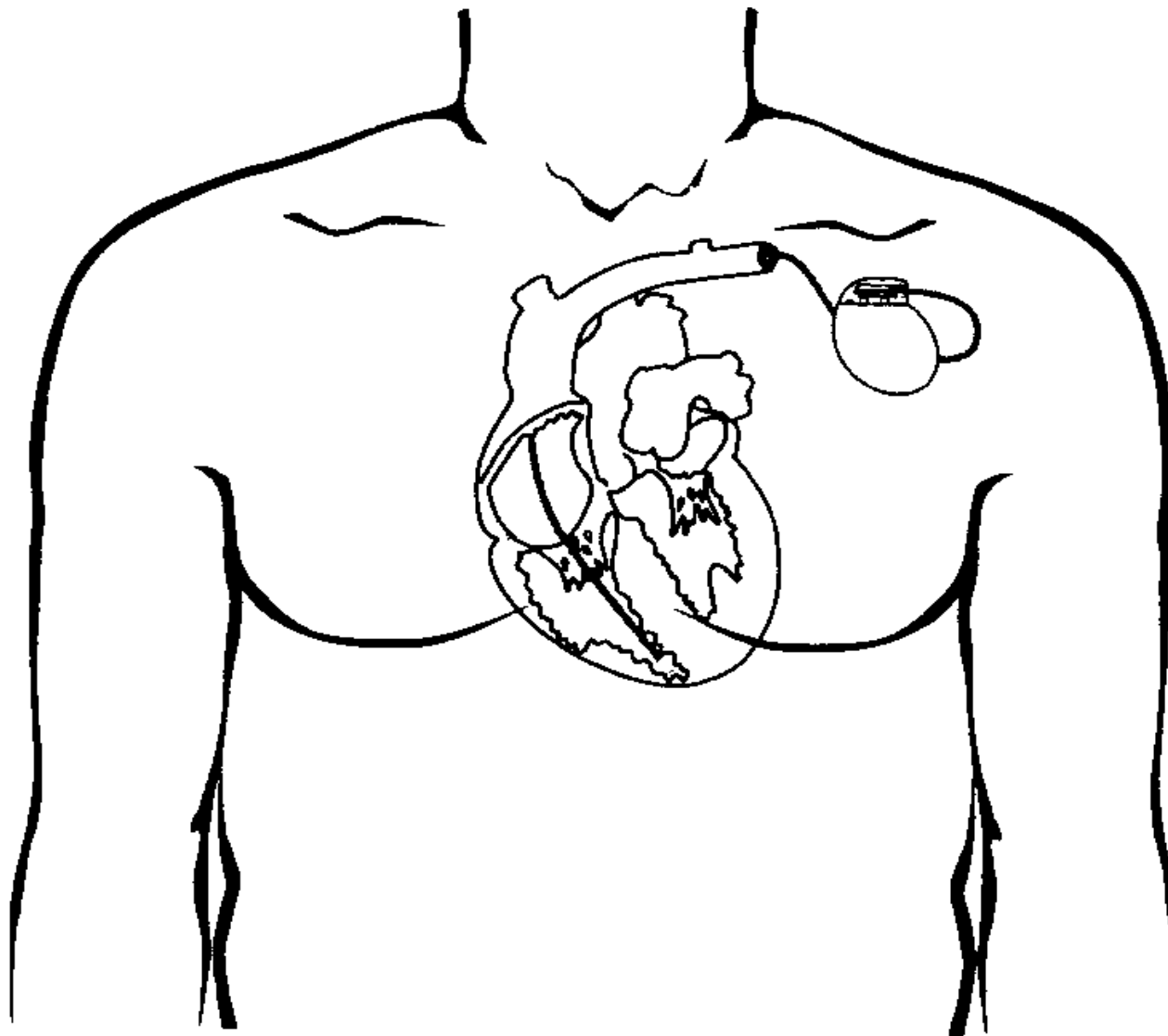


Figure 1. Implanted cardiac pacemaker

Demo Fuel Cells

0.02 ~ 10 W

H₂ , MeOH, Glucose, alcohols

PEM, Alkaline

NaBH₄ Fuel Cell



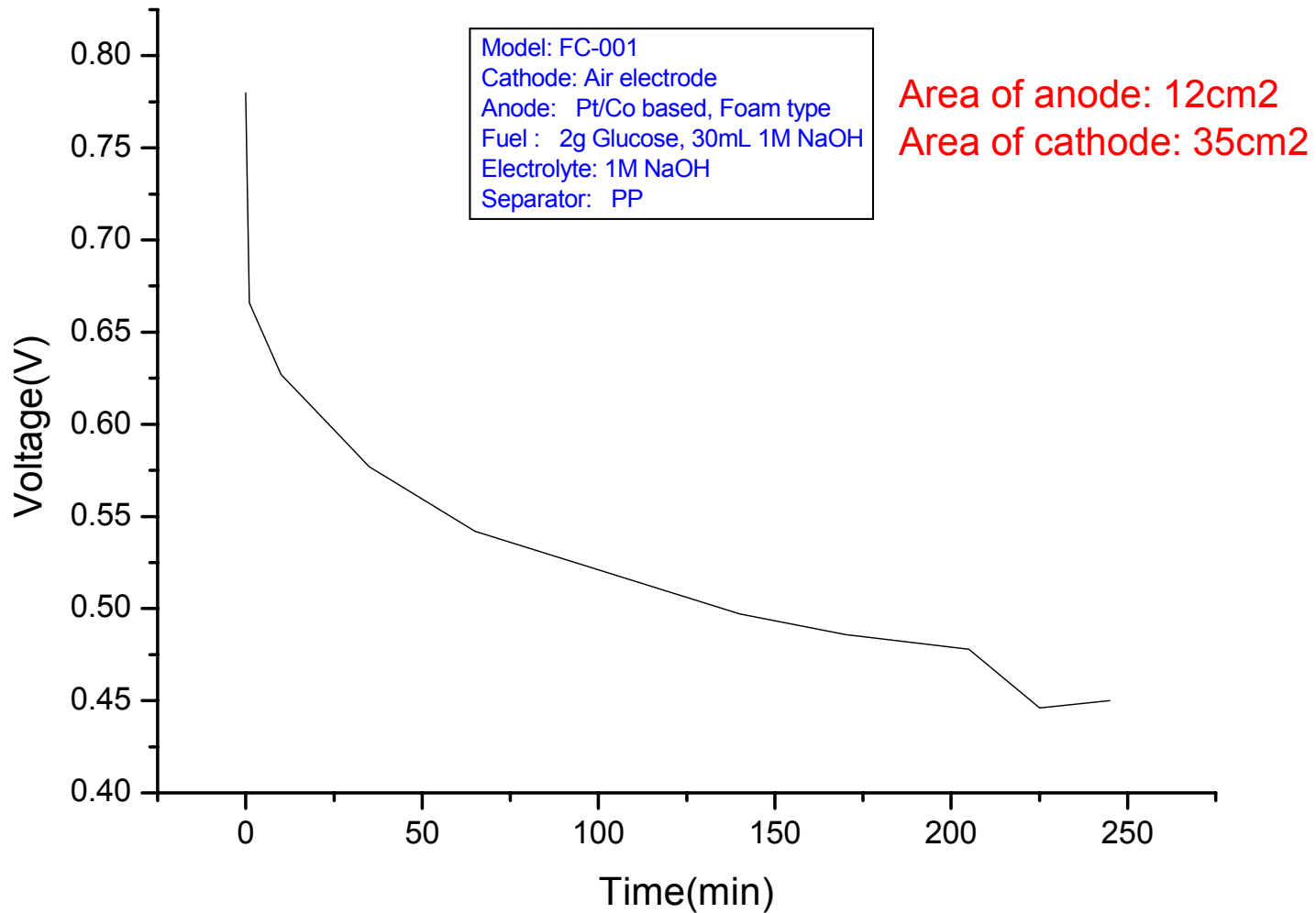


Features:

- 1) Leak Proof
- 2) Compact Design
- 3) Sandwich Type “MEA”
- 4) Transparent outlook
- 5) Easy to use
- 6) Low cost



Typical Performance of HKU-001





Power by 4 AA
6.0V, 200—300mA

Powered by 1AA, 1.5V
100—200mA

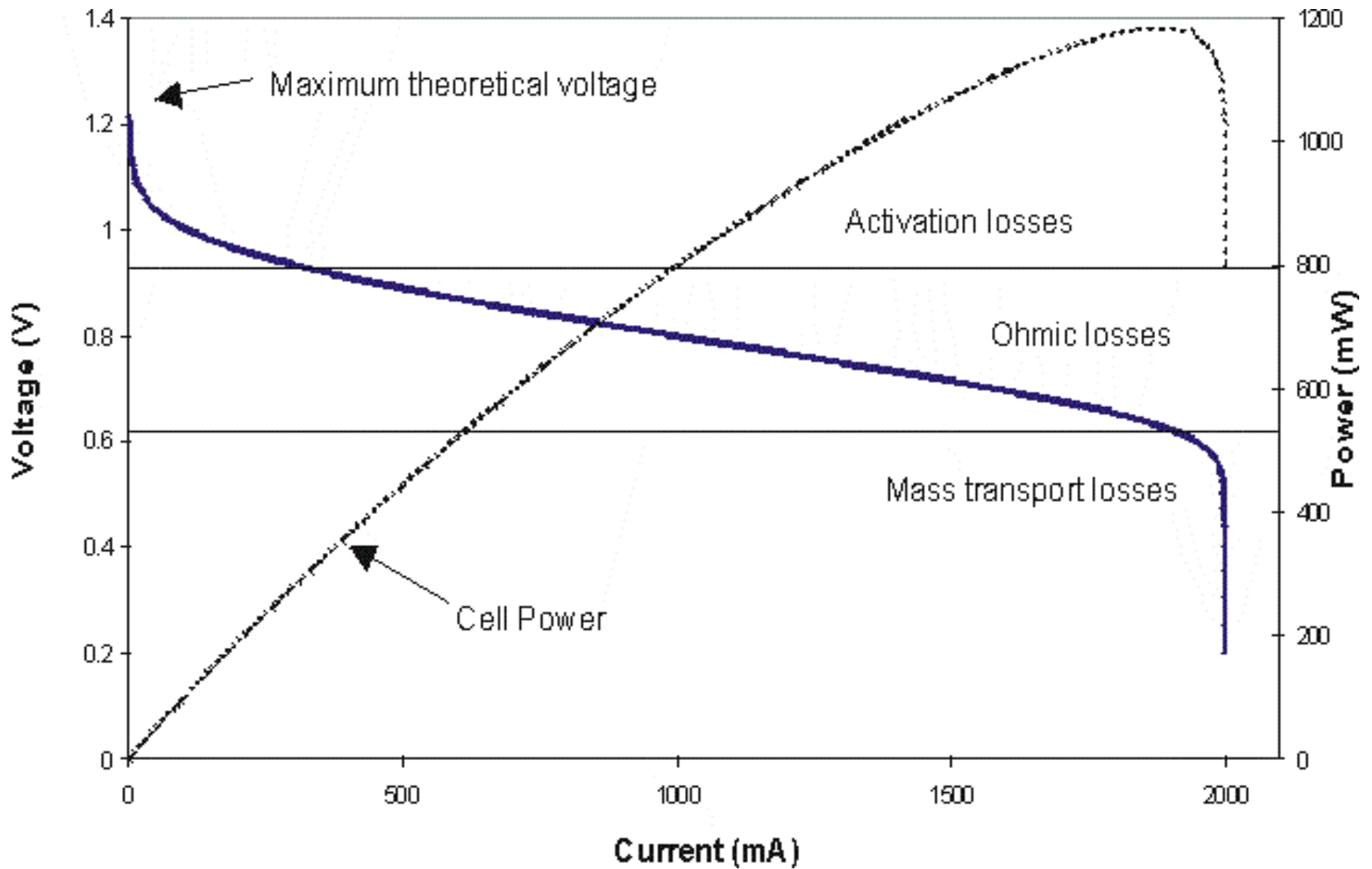


Toy R/C Market

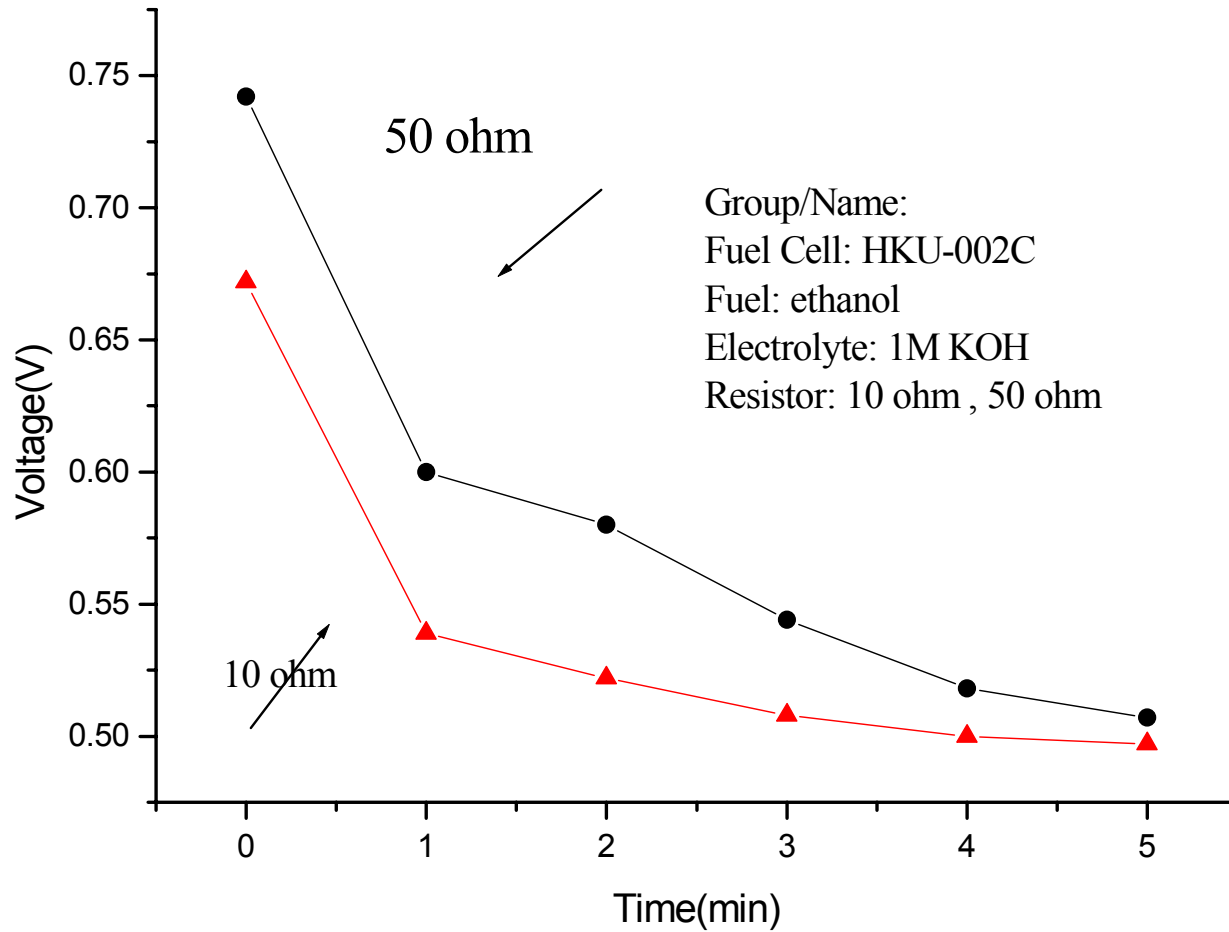
Sept 2003

Fuel Cells, K.Y. Chan, HKU

41



Voltage Response to different loadings



Electrolyte
:

Fuel Cell Used: HKU-002

Clock time	Time elapsed(min)	Voltage	Current(V/R: mA)
	0	OCV	
	1		
	2		
	3		
	4		
	5		